PHYSICS AND CHEMISTRY OF SOLID STATE

V. 22, No. 3 (2021) pp. 460-469

Section: Chemistry

DOI: 10.15330/pcss.22.3.460-469

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ФІЗИКА І ХІМІЯ ТВЕРДОГО ТІЛА Т. 22, № 3 (2021) С. 460-469

Хімічні науки

PACS: 64, 82.20 Hf

ISSN 1729-4428

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Application of Titanium Dioxide for Zirconium Ions Adsorption and Separation from a Multicomponent Mixture

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This work studies the adsorption of zirconium ions by the mesoporous titanium dioxide and by sodiummodified mesoporous titanium dioxide. Experimental maximal adsorption values of zirconium ions by H-TiO₂ and Na-TiO₂ were found to be 64 mg/g and 109.5 mg/g respectively. This process depends on the interaction time, the equilibrium concentration of zirconium ions, and the acidity of the solution. Adsorption kinetics fit well into the diffusion kinetic model and indicate several stages of zirconium ions adsorption. Equilibrium adsorption of zirconium ions is well described by Langmuir's adsorption theory for both adsorbents. The results obtained by inductively coupled plasma mass spectrometry showed that the investigated adsorbent selectively adsorb zirconium ions from the mixture with strontium and yttrium ions in the range of solution pH = 0 - 1. The percentage of maximum extraction of zirconium ions is 86.61 % for H-TiO₂ and 94.11 % for Na-TiO₂. This fact is extremely valuable for nuclear forensics or the determination of ⁹⁰Sr in low activity background samples.

Keywords: mesoporous TiO₂, zirconium ions, adsorption, separation, ICP-MS.

Received 16 July 2021; Accepted 15 August 2021.

Introduction

The relevance of studies of the adsorption of zirconium ions from aqueous solutions and its selective separation from strontium and yttrium can be explained by multiple factors. One of them is the determination of the low activity of 90Sr in environmental samples. Radioactive ⁹⁰Sr is a very harmful beta-emitter that accumulates in bones or fish scales [1] and may, significantly harm living organisms in which it accumulates due to the long halflife. Therefore, the maximum allowable levels of ⁹⁰Sr in the environment are extremely low [2], and their analysis is very difficult to perform. ⁹⁰Sr is a pure beta-emitter. Gamma spectrometry is unable to determine the amount of ⁹⁰Sr because it does not produce gamma lines. Its daughter nuclide 90Y also does not emit gamma rays. 90Y β - particles have higher maximum energy than β - particles of ⁹⁰Sr (2.281 MeV versus 0.546 MeV, respectively) and completely shield strontium. The amount of ⁹⁰Sr can be

approximately determined based on Vavilov-Cherenkov radiation generated by yttrium β - particles [3]. Another technique of environmental 90Sr measurement is the separation of ⁹⁰Sr from yttrium by the oxalate precipitation and subsequent determination of 90Sr amount based on the freshly formed daughter 90Y. This technique is used in the determination of the amount of 90Sr in aquatic ecosystems of the Chornobyl Exclusion Zone [1]. However, the accuracy of the oxalate technique is not very high and does not allow determining ⁹⁰Sr in low-level environmental samples. In this case, inductively coupled plasma mass spectrometry (ICP-MS) may be the only method of ⁹⁰Sr analysis. Several leading laboratories worldwide [4-6] use this method to analyze ⁹⁰Sr in the environment. The effectiveness of the ICP-MS method compared to other highly sensitive modern methods is presented in fig. 1.

This method of analysis is very sensitive (Fig. 1), but it diagnoses 90 Sr, 90 Y, and 90 Zr as a single peak at the mass



Fig. 1. Detection limits for common elemental techniques: **AA** - atomic absorption; **ICP-AES** - inductively coupled plasma atomic emission spectroscopy; **GFAAS** - graphite furnace atomic absorption; **ICP-MS** - inductively coupled plasma mass spectrometry (adapted from ref. [4]).

are spectroscopic interferences and overlap each other [4-6]. ⁹⁰Zr, the "granddaughter" of ⁹⁰Sr, hurts the mass spectrometry of ⁹⁰Sr samples, as described in [5]. Therefore, it is necessary to separate zirconium and strontium cations.

Nuclear forensic analysis is another application of zirconium adsorption and chemical separation from 90 Sr and 90 Y in combination with the ICP-MS analysis [7]. The isotopic ratio, measured using ICP-MS, serves as a radio chronometer and can be used to determine the date of fabrication of a 90 Sr - 90 Y radioactive source. The half-life of 90 Y is much shorter (64 hours) than that of 90 Sr (28.8 years). On elapse of time equal to several half-lives of yttrium, the amount of 90 Y becomes constant [8]. Therefore, for nuclear forensics, the important parameters are the number of 90 Sr ratio, thus methods of chemical separation of these elements become the main direction of scientific research in this field.

Adsorbents based on mesoporous TiO_2 showed high adsorption activity toward many cations, such as strontium, barium, zinc, cobalt, and yttrium [9-15]. The uniqueness of the properties of adsorbents based on mesoporous TiO_2 is due to the developed surface area and a large number of adsorption centers on it in combination with the predominantly crystalline structure of TiO_2 . These adsorbents are resistant to aggressive environments and thermally stable. The resistance of mesoporous TiO_2 to the action of acids is a very valuable characteristic, as it greatly simplifies the subsequent mass spectrometry of the studied solutions. The introduction of sodium cations into the structure of mesoporous TiO_2 leads to functional changes in the surface (for example, an increase in the number of active adsorption sites or shift of the point of zero charges), increasing the adsorption capacity of Na-TiO₂ compared to H-TiO₂ relative to heavy metal cations [12]. While the general laws of strontium ion adsorption process by adsorbents based on titanium dioxide are well studied, no surveys have been conducted of the adsorption of zirconium ions by these adsorbents yet.

This work will study the adsorption of zirconium ions by $H-TiO_2$ and $Na-TiO_2$, as well as the possibility of separation of ⁹⁰Sr and ⁹⁰Zr isotopes by investigated adsorbents for subsequent analysis using inductively coupled plasma mass spectrometry.

I. Experimental Techniques

1.1. Synthesis of H-TiO2 and Na-TiO2 adsorbents

Experimental samples of anatase modification titanium dioxide with protonated and sodium-modified surface were obtained by sol-gel method, using a solution of titanium aqua complex [Ti(OH₂)₆]³⁺·3Cl⁻ as a precursor [12]. The 0,1M solution of titanium precursor was heated at 60 °C for 60 minutes to prepare titanium dioxide with a protonated surface (H-TiO₂). Globular particles of TiO₂ with a diameter of 4 - 5 nm were formed in the reaction medium, due to the hydrolysis of the precursor, and condensation of the molecules Ti(OH)₄·2H₂O. The 10 % NaOH solution was added dropwise to the dispersion to deoxidize the resulting product. At pH ~ 5.3 the dispersion thickened rapidly because of gel formation. The hydrogel with a pH of \sim 7.0 was washed with distilled water from the adsorbed impurities of Na⁺, Cl⁻ ions. Then, it was dried for 4 hours, at a temperature of 140°C.

Titanium dioxide with a sodium surface was obtained by contacting globular TiO_2 particles with 10 % NaOH solution. The TiO_2 dispersion was kept in an alkali medium (pH ~ 12) for 3 hours at room temperature, then the dispersion was washed with distilled water. Washing and decantation of the dispersion were repeated at least 5 times, and after establishing the pH ~ 7, it was dried at a temperature of 140 °C. The main textural characteristics of the adsorbents are shown in Table 1.

1.2. Batch adsorption studies

Recommendations for the separation of elements can be made after studying the general patterns of the process of adsorption of the studied elements. Studies of the adsorption capacity of H-TiO₂ and Na-TiO₂ toward zirconium cations were performed under batch conditions. The weight of the adsorbent was 50 mg, and the volume of the ZrOCl₂ aqueous solution was 5 ml. The influence of time interaction, the equilibrium concentration of the zirconium ions, and the acidity of the solution was investigated. Initial and residual concentrations of

Table 1

The textural characteristics of investigated samples, according to [12]

Sample	$\frac{S_{BET}}{(m^2g^{-1})}$	S_{micro} (m^2g^{-1})	$S_{\text{meso}},$ $(m^2 \text{g}^{-1})$	$\begin{array}{c} V_{p}, \\ (cm^{3}g^{-1}) \end{array}$	V_{micro} (cm ³ g ⁻¹)	V _{meso} (cm ³ g ⁻¹)	$\mathbf{pH}_{\mathbf{pzc}}$
H-TiO ₂	349	129	230	0.191	0.061	0.130	5.35
Na-TiO ₂	239	100	139	0.152	0.054	0.098	9.42

zirconium ions were determined using direct complexometric titration in a strongly acidic medium with Xylenol Orange as an indicator [16]. Adsorption values were calculated using (eq.1) as follows:

$$q_e = \frac{\left[(C_o - C_e)V\right]}{m} \quad , \tag{1}$$

where q_e – is the amount of adsorbate uptake, mg/g; C_o and C_e – are initial and residual concentrations of adsorbate, mg/L; V - is solution volume, L; m - is mass of adsorbent, g [17].

The influence of solution acidity on zirconium cations adsorption by investigated adsorbents was studied under the same conditions, however, the volume of the solution was 10 ml (5 ml of $ZrOCl_2$ solution and 5 ml of the medium) and the mass of the adsorbent remained unchanged.

The most commons adsorption kinetic models were applied to experimental data: kinetic models based on pseudo-first, pseudo-second-order equations; Elovich and diffusion kinetic models. However, special attention was paid to the Elovich model ($q_t = f(\ln t)$) and the diffusion kinetic model ($q_t = f(t^{0.5})$), as they allow predicting the mechanism of adsorption: mainly physical (diffusion model), or chemisorption (Elovich model) [18-23]. Langmuir and Freundlich's adsorption theories were used to analyze the equilibrium adsorption. The equations of these theories (2) and (3) are given below:

$$q_e = \frac{A_{maxKC_e}}{1+KC_e},\tag{2}$$

$$q_e = K_f \times C_e^n, \tag{3}$$

where, A_{max} (mg/g) – maximum adsorption value, which corresponds of fill in the whole adsorption centers; K_L (L/mg) – Langmuir constant; C_e (mg/L) – adsorbate equilibrium concentration; q_e (mg/g) – quantities of adsorbate uptake at equilibrium; K_f – Freundlich constant, $\frac{mg/g}{L}n$; n- Freundlich intencity parameter.

Separation factor $\alpha_{Sr, Zr}$ of strontium and zirconium was calculated according to [7]:

$$\alpha_{Sr,Zr} = \frac{Intensity \, [Cps] 88 - Sr}{Intensity \, [Cps] 90 - Zr}, \tag{4}$$

where Intensity in [count per second] was experimentally measured value by ICP-MS of corresponding isotopes after adsorption.

Nonlinear approximation of experimental results was processed in the "Solver add-in" to Microsoft Office Excel. The chi-squared test is highly recommended for the nonlinear method to confirm the best fitting isotherm for a given adsorption system. High χ^2 indicates high divergence between the experiment and the model. The chi-square value χ^2 and coefficient of determination R² were calculated using equations (5) and (6). In general, the recommendations from the publication [20] were used in the analysis of experimental adsorption results.

$$R^{2} = 1 - \frac{\Sigma(q_{e,exp}, -q_{e,calc})^{2}}{\Sigma(q_{e,exp}, -q_{e,mean})^{2}},$$
 (5)

$$\chi^2 = \sum \frac{(q_{e,exp} - q_{e,calc})^2}{q_{e,calc}} .$$
 (6)

1.3. ICP-MS analysis of separation of investigated cations

The study of the possibility of strontium, yttrium, and zirconium ions separation using the investigated adsorbents was performed under batch conditions. The ⁸⁸Sr, ⁸⁹Y, ^{90,91}Zr isotopes were analyzed by the inductively coupled plasma mass spectrometer (ICP-MS) [4-6] 'Element 2' with argon plasma, located in the Nuclear Forensics laboratory of KINR, Kyiv. The study was performed with a mixture of the high purity standards solutions (High Purity Standards, USA) of the corresponding elements.

The results were measured in the number of [CPS] pulses "count per second" relative to m/z.

As has been said above, ⁹⁰Y does not play a significant role in determining the date of fabrication of a ⁹⁰Sr -⁹⁰Y radioactive source. This is due to the fact, that the half-life of ⁹⁰Y is much shorter (64 hours) than the half-life of ⁹⁰Sr (28.8 years) and its amount throughout the life of ⁹⁰Sr remains constant. This statement can be illustrated by formulas (7) - (9):

$$\lambda_2 - \lambda_1 \cong \lambda_2,\tag{7}$$

Where λ_2 , – Decay constant of ⁹⁰Y; λ_1 , – decay constant of ⁹⁰Sr.

The number of daughter nuclei is related to the number of parent nuclei by the equation (7):

$$N_{Y} = \frac{\lambda_{1}}{\lambda_{2} - \lambda_{1}} \times N_{Sr} \left(e^{-\lambda_{1}t} - e^{-\lambda_{2}t} \right) \cong$$
$$\cong \frac{\lambda_{1}}{\lambda_{2}} N_{Sr} \left(1 - e^{-\lambda_{2}t} \right)$$
(8)

After several half-lives, an equilibrium establishes and the amount of 90Y can be calculated:

$$N_Y = \frac{\lambda_1}{\lambda_2} (N_{Sr})$$
, or $\frac{N_Y}{(T_{1/2})^2} = \frac{N_{Sr}}{(T_{1/2})^1}$, (9)

$$\lambda_2, \left(T_{\frac{1}{2}}\right) 2$$
 - Half-life of ⁹⁰Y;
 $\lambda_1, i \left(T_{\frac{1}{2}}\right) 1$ -- Half-life of ⁹⁰Sr.

Stable ⁸⁹Y, in contrast to ⁹⁰Y, plays a significant role, because it was very often used as a carrier for radioactive ⁹⁰Sr and ⁹⁰Y. This was because, the separation of ⁹⁰Sr from a mixture of fission radionuclides, during fabrication of a 90Sr -90Y radioactive source, was carried out by the reaction of precipitation of strontium and yttrium with oxalates [1]. Stable ⁸⁹Y in the result ⁹⁰Sr-⁹⁰Y source may be at a high concentration. It can affect the selective adsorption of Sr^{2+} or Zr^{4+} because the cations Y^{3+} are also adsorbed on the surface of titanium dioxide. Therefore, a mixture of isotopes of ⁸⁸Sr, ⁹⁰Zr, ⁹¹Zr, and ⁸⁹Y was subjected to the analysis by ICP-MS. A great advantage of ICP-MS is its multi-element capability, which allows multiple elements to be measured simultaneously in a single analysis. However, interferences need to be controlled. Internal standardization is usually employed to

correct for changes in instrument operating conditions and sample-specific matrix effects. According to recommendations, which were given in publication [5], the internal standard will have a similar mass and ionization potential to the analyte (⁸⁸Sr, ⁸⁹Y, ⁹⁰Zr, ⁹¹Zr). Therefore, ¹⁰³Rh was chosen, as an internal standard. External calibration of the ICP-MS was performed using calibration Standard A, containing known concentrations of the elements. The error due to the formation of polyatomic ions ⁸⁹Y¹H in plasma was determined using Standard 1. Standard 1 is a mixture of about 10 ng ⁸⁸Sr and ⁸⁹Y. Standard solution 2 (Standard 2) was a mixture of ⁸⁸Sr, ⁸⁹Y, ⁹⁰Zr, ⁹¹Zr, which was divided into 5 equal parts, four of them were mixed with adsorbents, and the fifth was left as a control solution. In addition, Standard 3 was pure 2 % HNO₃ 'Optima'.

Adsorption and separation of strontium, yttrium, and zirconium ions were performed in batch conditions for an hour. Mass of adsorbents was 100 mg, volume of solutions – 10 ml. After adsorption, the adsorbents were separated from the solution by filtration. The slow-filtering paper with dense narrow pores for finest deposits was selected for this purpose. Selective adsorption of zirconium and the possibility of separation of zirconium from strontium and yttrium were evaluated by analyzing the isotopes ⁸⁸Sr, ⁸⁹Y, ⁹⁰Zr, ⁹¹Zr, and ¹⁰³Rh by ICP-MS at least three times.

II. Results and Discussion

2.1. Adsorption of zirconium ions by $H-TiO_2$ and $Na-TiO_2$

The results of the dependence of the zirconium adsorption values by $H-TiO_2$ and $Na-TiO_2$ on agitation time are shown in Fig. 2.



Fig. 2. Dependence of the adsorption values of zirconium ions by H-TiO₂ and Na-TiO₂ on the agitation time.

The results, which are shown in Fig. 3 and Table 2, indicate that the diffusion model best describes the process of adsorption of zirconium ions by the investigated adsorbents. According to the results of the analysis, the zirconium ions adsorption by H-TiO₂ and Na-TiO₂ occurs in several stages: diffusion from solution to the surface of the adsorbent's surface (Step 1 'bulk transport'); diffusion on the adsorbent's surface (Step 2 'film diffusion') and diffusion deep into the pores of the adsorbent (Step 3 'intraparticle diffusion'). The highest diffusion coefficients (k_{ipd}) were



Fig. 3. Application of kinetic models to experimental results of zirconium ions adsorption by H-TiO₂ and Na- TiO₂: (a) Pseudo-second; (b) Elovich; (c) Pseudo-first; (d) Intra-particle diffusion kinetic models.

by H-11O ₂ and Na- 11O ₂								
Model	Adsorbent	Equation	Parameters	\mathbb{R}^2				
Pseudo-first	H-TiO ₂	$\log(q_0 - q_t) = -0.035t + 2.035$	k _{1 =} 0.035	0.8952				
	Na-TiO ₂	$log(q_0-q_t) = -0.035t+1.98$	$k_1 = 0.035$	0.9365				
Pseudo-	H-TiO ₂	$t/q_t = 0.019t + 0.49$	k2=0.019	0.8664				
second	Na-TiO ₂	$t/q_t = 0.0128t + 0.27$	$k_2 = 0.0128$	0.9511				
Elovich	H-TiO ₂	$q_t = 19.33 \ln t - 29$	α =4.32;β=0.0517	0.9155				
	Na-TiO ₂	$q_t = 18.17 \ln t - 29$	α=6.82; β=0.055	0.902				
Difussion	H-TiO ₂	$q_t = 2.52 t^{0.5} + 19$	k _{ipd} =2.52; C =19	0.999				
Step 1	Na-TiO ₂	$q_t = 2.78 t^{0.5} + 9.4$	k _{ipd} =2.78; C =9.4	0.999				
Step 2	H-TiO ₂	$q_t = 5.14 t^{0.5} + 20.7$	k _{ipd} =5.14; C =20.7	0.9723				
	Na-TiO ₂	$q_t = 7.79 t^{0.5} - 5.47$	$k_{ipd} = 7.79$	0.9446				
Step 3	H-TiO ₂	$q_t = 0.768 t^{0.5} + 52$	k _{ipd} =0.768; C =52	0.999				
	Na-TiO ₂	$q_t = 0.072 t^{0.5} + 50$	k _{ipd} =0.072; C=50	0.999				

Application of kinetic models to experimental results of zirconium ions adsorption by H-TiO₂ and Na-TiO₂

 q_o and q_t (mg/g) - adsorption capacity at equilibrium and time t. respectively; $k_1(\min^{-1})$. k_2 (g·mg⁻¹ min⁻¹) rate coefficients of pseudo-first order equation and pseudo-second order equation. D_{ipd} (mg/g min^{0.5}) – coefficient of intra-particle diffusion; β (mg/g)- desorption constant. α (mg/g min) – rate coefficients of Elovich equation.

observed during the diffusion of zirconium ions along the surface of H-TiO₂ and Na-TiO₂. The values of the constant C mg/g in the equations of the diffusion model are related to the thickness of the boundary layer [20]. The larger value of C means the greater effect of the thickness of the boundary layer on the adsorption of zirconium ions. When zirconium ions diffuse along the Na-TiO₂ surface, the boundary layer does not affect the adsorption. In all other cases, the values of C are significant, so the thickness of the boundary layer of the adsorbent surface affects the process of adsorption of zirconium ions from the neutral medium. For the adsorbent H-TiO₂, the value of C increases in the series Step 1-Step 2-Step 3 and has a value of 19 mg/g; 20.7 mg/g, and 52 mg/g, respectively.

2.2. Equilibrium adsorption of zirconium ions by H-TiO₂ and Na- TiO₂ and influence of solution acidity on the adsorption process

The results of equilibrium studies of zirconium ions adsorption by H-TiO₂ and Na-TiO₂ are shown in Fig. 4 and Fig. 5. The application of the Langmuir and Freundlich theories to the experimental results is given in Table 3.

The experimental isotherms of zirconium ions adsorption by the studied adsorbents are better described by Langmuir's theory than by Freundlich's theory for both adsorbents. However, the divergence between the experimental results and calculated by Langmuir theory (χ^2) for Na-TiO₂ are higher. The main differences between the experimental values and the theoretically calculated ones for zirconium ions adsorption by the Na-TiO₂ are in the region of low equilibrium concentrations of the adsorbate. This can be explained by the very active surface of the adsorbent. In our opinion, this is the reason for rather high values of χ^2 . The values of the maximum adsorption of zirconium ions calculated according to Langmuir theory are in good agreement with the experimentally determined ones (Table 3) and are lower than the values of adsorption of strontium ions by the H-TiO₂ and Na-TiO₂ [12]. The maximum adsorption values



Fig. 4. Isotherm of zirconium ions adsorption by H-TiO₂; nonlinear approximation by Langmuir and Freundlich theories.



Fig. 5. Isotherm of zirconium ions adsorption by Na-TiO₂; nonlinear approximation by Langmuir and Freundlich theories.

Table 3

Adsorption process	Theory	Parameters of equation of corresponding theory	Calculated q _{max} , mg/g	R ²	χ²
$Zr^{4+} by H-TiO_2$ $q_{e exp} = 61.4 mg/g$	Langmuir	$K_L = 0.00318$ $A_{max} = 70.46$	64.23	0.8544	15.11
	Freundlich	$K_f = 4.458$ n = 0.338	68.73	0.7747	26.78
Zr ⁴⁺ by Na-TiO ₂	Langmuir	$K_L=0.00169$ $A_{max} = 128.99$	109.1	0.9166	16.17
$q_{e exp} = 109.5 \text{ mg/g}$	Freundlich	$K_f = 3.893$ n = 0.4188	114.9	0.8862	14.27

Application of the Langmuir and Freundlich theories to the experimental equilibrium adsorption of zirconium ions by H-TiO₂ and Na-TiO₂

Table 4

Values of self-diffusion coefficients of Zr (IV) and Sr (II) ions in aqueous solutions with different pH according to publication [25]

pH	Zr(IV) D 10 ⁻⁵ cm ² /s	Zr(IV) radius, Å	Sr(II) D 10 ⁻⁵ cm ² /s	
9M	0.3 ± 0.016	4.8	5.58 ± 0.08	
6M	0.345 ± 0.005	4.8	6.0 ± 0.13	
3M	0.42 ± 0.007	4.8	6.23 ± 0.07	
2M	0.46 ± 0.01	4.8		
1M	0.48 ± 0.014	4.8		
0.4 M	0.488 ± 0.003	4.8		
0.1 M	0.351 ± 0.006	7.0		
pH = 2	0.205 ± 0.011	11	7.75 ± 0.04	
pH - 2.8	0.137 ± 0.004	12		
pH = 4.2	0.056 ± 0.004	44		
pH = 7.5	0.05 ± 0.009	50	7.79 ± 0.1	
pH = 8.2	0.115 ± 0.004	21		
pH = 10.4	0.106 ± 0.021	23		
pH = 11.5	0.13 ± 0.01	19	7.58 ± 0.06	

of the strontium ions in the neutral medium are 78.4 mg \cdot g⁻¹ by H-TiO₂ and 208.4 mg \cdot g⁻¹ by Na-TiO₂ and the maximum adsorption of zirconium ions are 61.4 mg \cdot g⁻¹ by H-TiO₂ and 109.5 mg \cdot g⁻¹ by Na-TiO₂. The reason for the lower adsorption of zirconium ions compared to strontium ions in aqueous solutions with a neutral pH may be the high tendency of zirconium cations to hydrolysis [24, 25].

The plot, shown in Fig. 6 indicates that the weakest adsorption of zirconium ions occurs in a neutral medium. The tendency of zirconium cations to hydrolyze [20, 21] determines the large size of hydrolyzed zirconium ions and their low mobility in solution and, accordingly, insignificant adsorption.

The results presented in Fig. 6 are in good agreement with the literature data on the mobility and size of zirconium ions in solution, shown in Table 4. For comparison, the table shows the values of the mobility of strontium cations, as well. The concentration of the corresponding ions was 10^{-5} mole/L; studies were performed using HCl, NH₄OH, and 100-fold excess of electrolyte NH₄Cl.



Fig.6. pH dependence of zirconium ions adsorption by H-TiO₂ and Na-TiO₂

2.3. Selective adsorption of zirconium ions from the mixture

Schematically, the experiment on the adsorption separation of strontium, yttrium, and zirconium ions is shown in Fig. 7.

The results presented in Tables 5 and 5 (a) indicate the selective adsorption of zirconium ions from a mixture of strontium and yttrium ions. This process is illustrated in Figs. 8 (a) and (b). The results in Table 5 (a) indicate that the amount of strontium, yttrium and internal rhodium ions was not changed after interaction with adsorbents. This fact evidences the absence of adsorption of these elements under experimental conditions. Analysis by ICP-MS showed that the error due to the formation of ⁸⁹Y¹H polyatomic ions is 1210 counts per second at a mass of 90amu. In addition, the number of contaminants of ⁸⁸Sr and ⁹⁰Zr in the used solvent was recorded. If we take into account all these contributors to the mass peak of 90amu and subtract the background number of counts from ⁹⁰Zr, the percentage of extracted ⁹⁰Zr will be 86.61 % for H-

TiO₂ and 94.11 % for Na-TiO₂.

Figures 8 (a) and (b) illustrate the selective adsorption of zirconium ions by H-TiO₂ and Na-TiO₂ from nitric acid with HF micro-impurities in the absence of adsorption of strontium and yttrium ions. The amount of strontium ions even slightly increases due to the ⁸⁸Sr contaminated micro impurities (Fig. 8 (a)).

Selective zirconium ion adsorption is observed in the range of solutions acidity pH = 0 - 1. This range of solution acidities is below the pHpzc of the studied adsorbents (Table 1). The number of adsorption centers (\equiv TiO-) able to bind cations is slightly reduced and the surface of H-TiO₂ or Na-TiO₂ has an overall positive charge in the experimental conditions, although some areas are still able to bind cations on the adsorbent surface. The overall positive surface charge of H-TiO₂ or Na-TiO₂ becomes a Coulomb barrier for the adsorption of relatively large, positively charged ions of divalent strontium and trivalent yttrium. Therefore, strontium and yttrium ions were not adsorbed by these adsorbents in the 0.32M HNO₃ medium. It should be noted, that at pH values closer to a



Fig. 7. Scheme of the experiment of separation of strontium, yttrium and zirconium ions and subsequent ICP-MS analysis.

Table 5

C initial 90-Zr (Standard 2)		Adsor- bent	Intensity [cps] After	Adsorption 90-Zr		C residual, 90-Zr	Uncertaintie s 89Y1H [cps]	α Sr,Zr
Inten-sity [cps]	ng		adsorption	ng	%	lig	1210	
1057427	5.094	H-TiO ₂	156695±554	4.3392	85.18	0.7548	1210	25.63
2229000	6.46	Na-TiO ₂	146506±768	6.0355	93.42	0.4245		27.42

Results of selective adsorption of zirconium ions by H-TiO2 and Na-TiO2

Table 5 (a)

Amounts of ⁸⁸ Sr, ⁸⁹ Y and ¹⁰³ Rh before and after adsorption									
Isotop	C initial (Standard 2)		Adsorbent	Intensity [cps] After	Intensity [cps]	Uncertainties ⁹⁰ Zr Standard 3 [cps]			
	Intensity [cps]	ng		adsorption	Standard 3				
88-Sr	2101905	9.9	H-TiO ₂	4017586	510471				
89-Y	2431139	10	H-TiO ₂	3179047	9245	14588			
88-Sr	10413000	14.5	Na-TiO ₂	10027000	14588				
89-Y	5715000	12.5	Na-TiO ₂	4663000	1768.8				
103-Rh	516693	3	$H-TiO_2(Na-TiO_2)$	448009	-				



Fig. 8 (a). ICP-MS spectra of a solution containing about 10 ng of strontium, yttrium, and zirconium ions, before and after adsorption by H-TiO₂.



Fig. 8 (b). ICP-MS spectra of a solution containing about 10 ng of strontium, yttrium, and zirconium ions, before and after adsorption by Na-TiO₂.

neutral or alkaline environment, the adsorption of strontium ions by these adsorbents is extremely intense [9-14]. Ionic radius of Zr^{4+} is smaller than the corresponding value of Sr^{2+} or Y^{3+} (0.84 Å compared to 1.02 Å for Y^{3+} and 1.26 Å for Sr^{2+} ions) [26]. Zirconium loses its hydrate shell under such acidity of the solution. This fact allows zirconium ions to neglect electrostatic repulsion and interact with residual cation-bonding adsorption cites of the adsorbents. On the other hand, the mobility of zirconium ions [25]. Therefore, after approaching the surface of TiO₂, zirconium generally remains in the adsorbed state.

The obtained results are promising for the separation of ⁹⁰Sr and ⁹⁰Zr isotopes. The absence of adsorption of

strontium and yttrium ions under such extreme solution acidity indicates that zirconium ions can be selectively adsorbed even with an excess of cations of alkaline earth elements and elements of the YRE group. The resistance of TiO₂ to the acidic media allows direct one-stage separation of zirconium ions without additional procedures for the separation of alkaline earth elements and lanthanides, which can shift the initial ratio of 90 Sr/ 90 Zr [27-29]. This fact is extremely valuable for nuclear forensics or the determination of 90 Sr in low activity background samples.

Conclusion

The adsorption of zirconium ions by titanium dioxide has been studied. The dependence of this process on the agitation time, the equilibrium concentration of the zirconium ions, and the acidity of the solution have been established.

The kinetics of zirconium ions adsorption by $H-TiO_2$ and Na-TiO₂ is stepwise and fitting well with the diffusion kinetic model.

Experimental maximum values of adsorption of zirconium ions by the studied adsorbents are $61.4 \text{ mg} \cdot \text{g}^{-1}$ for H-TiO₂ and 109.5 mg \cdot \text{g}^{-1} for Na-TiO₂. These values are in good agreement with the calculated values of the maximum adsorption according to Langmuir's theory.

Separation of strontium and zirconium ions was performed. The residual solution was analyzed by ICP-MS. It was shown that the investigated adsorbents selectively adsorb zirconium ions from the mixture with strontium and yttrium ions in the range of solution pH = 0 - 1. The percentage of maximum extraction of zirconium ions is 86.61 % for H-TiO₂ and 94.11 % for Na-TiO₂. This fact is extremely valuable for nuclear forensics or the determination of ⁹⁰Sr in low activity background samples.

Funding

This work was supported by a research grant in Nuclear Forensics. STCU [Project 9906].

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- [1] I.F. Mironyuk, I.M. Mykytyn, O.Ye. Kaglyan, D.I. Gudkov, Nucl. Phys. At. Energy 21(4) 347 (2020); https://doi.org/10.15407/jnpae2020.04.347.
- Public health statement: strontium. https://www.atsdr.cdc.gov/ ToxProfles/tp159-c1-b.pdf. Accessed 1 Feb (2019).
- [3] Kevin John Swearingen, Nathalie A. Wall, Journal of Radioanalytical and Nuclear Chemistry 320, 71 (2019); https://doi.org/10.1007/s10967-019-06444-6.
- [4] N. Kavasi, S.K. Sahoo, H. Arae, T. Aono, Z. Palacz, Nature Scientific Reports 9, 16532 (2019); <u>https://doi.org/10.1038/s41598-019-52890-3.</u>
- [5] Scott C. Wilschefski, Matthew R Baxter, Clin. I. Biochem Rev 40(3) 115 (2019); https://doi.org/10.33176/AACB-19-00024.
- [6] G. Favre, R. Brennetot, et al., International Journal of Mass Spectrometry 265(1) 15 (2007); https://doi.org/10.1016/j.ijms.2007.04.012.
- [7] Zattoni Ana Paula, Separation and Analysis of Sr-90 and Zr-90 for Nuclear Forensic Applications. (Laval University, Quebec, Canada, 2015); <u>31654.pdf (ulaval.ca) http://hdl.handle.net/20.500.11794/26052.</u>
- [8] Hendee William R., Ritenour E. Russel, Medical Imaging Physics, 4th edition. (A John Wiley &Sons inc. publication, New York, 353, 2002). ISBN: 9780471221159; <u>https://www.doi.org.10.1002/0471221155.</u>
- [9] I. Mironyuk et al., Journal of Molecular Liquids, 282, 587 (2019); <u>https://doi:10.1016/J.MOLLIQ.2019.03.026</u>.
- [10] I. Mironyuk et al., Journal of Environmental Chemical Engineering 7(6) 103430 (2019); https://www.doi.org/10.1016/j.jece.2019.103430.
- [11] I. Mironyuk et al., Journal of Molecular Liquids, 285, 742 (2019); https://www.doi.org/10.1016/j.molliq.2019.04.111.
- [12] I. Mironyuk, I. Mykytyn, H. Vasylyeva, Kh. Savka, Journal of Molecular Liquids 316(10) 113840 (2020); https://www.doi.org/10.1016/j.molliq.2020.113840.
- [13] I.F. Mironyuk, H.V. Vasylyeva, Sorption removal of Sr²⁺ and Y³⁺ ions from aqueous solutions by a TiO₂ based sorbent. RAD Conf. Proc. 3 (2018). P.15; <u>https://doi.org/10.21175/RadProc.2018.04.</u>
- [14] H. Vasylyeva, I. Mironyuk, I. Mykytyn, Kh. Savka, Applied Radiation and Isotopes 109473 (2020); <u>https://doi.org/10.1016/j.apradiso.2020.109473.</u>
- [15] H. Vasylyeva, I. Mironyuk, I. Mykytyn, Chemistry, physics, and technology of surface 10(4) 446 (2019); https://www.doi.org:10.15407/hftp10.04.446.
- [16] G. Schwarzenbach, H. Flaschka, Complexometric titrations. Translated [from the German] and rev. in collaboration with the authors by H.M.N.H. (Irving, London, Methuen, P. 490 (1969). ISBN: 0416192904 9780416192902.
- [17] Arthur W. Adamson, Physical chemistry of surfaces (3rd edition) (Wiley-Interscience, New York, 698, 1976); <u>https://doi.org/10.1002/pol.1977.130151014.</u>
- [18] W. Plazinski, W. Rudzinski, A. Plazinska, Advances in Colloid and Interface Science 152(1-2), 2 (2009); <u>https://doi.org/10.1016/j.cis.2009.07.009</u>.
- [19] F.-Ch. Wu, R.-L. Tseng, R.-Sh. Juang, Chemical Engineering Journal 150(2-3), 366 (2009); https://doi.org/10.1016/j.cej.2009.01.014.
- [20] H.N. Tran, S-J. You, A. Hosseini-Bandegharaei, H-P. Chao, et al., Water Res. 120, 88 (2017).
- [21] Fatin Izzaidah Anuar, Tony Hadibarata, Muhammad Syafrudin, Zahra Fona, Biointerface Research in Applied Chemistry 10(1), 4774 (2020); ISSN 2069-5837; <u>https://doi.org/10.33263/BRIAC101.774779.</u>
- [22] Shivashanggeeta Kanthasamy, Tony Hadibarata et al., Biointerface Research in Applied Chemistry 10(1), 4706 (2020); ISSN 2069-5837; <u>https://doi.org/10.33263/BRIAC101.706713.</u>
- [23] H. Vasylyeva, I. Mironyuk, M. Strilchuk, et al., Biointerface Research in Applied Chemistry 11(5), 13421 (2021); <u>http://dx.doi.org/10.33263/BRIAC115.1342113431.</u>
- [24] Atlas of Eh-pH diagrams, (2005). Intercomparison of thermodynamic databases Geological Survey of Japan Open-File Report No.419.
- [25] V.E. Staryk et al., Radiochemistry,6(4), 468 (1964). (in Russian).
- [26] K.M. Mackay, R.A. Mackay, W. Henderson, Introduction to modern inorganic chemistry 5th edition (Blackie Academic and professional, and imprint of Chapman and Hall, 2-6 Boundary Row, London SE1 8NH, UK, (1996); ISBN 0751403733.
- [27] McLain Derek R., Amato Victoria, Sudowe Ralf, J Radioanal. Nucl. Chem. 314(3) 15 (2018); https://www.doi.org:10.1007/s10967-017-5599-x.
- [28] Zsolt Varga, Adrian Nicholl, Maria Wallenius, Klaus Mayer, J. Radioanal. Nucl. Chem. 307, 1919 (2015); <u>https://www.doi.org.10.1007/s10967-015-4418-5.</u>
- [29] J.L. Steeb, D.G. Graczyk, Y. Tsai, et al., J. Anal. At. Spectrom. 28, 1493 (2013); https://pubs.rsc.org/en/journals/journal/ja.

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Використання діоксиду титану для адсорбції йонів цирконію та виділення їх із багатокомпонентної суміші

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Дана робота присв'ячена дослідженням адсорбції йонів цирконію мезопористим діоксидом титану та діоксидом титану із натрованою поверхнею. Експериментально визначені величини максимальної адсорбції йонів цирконію складають 64 мг/г та 109,5 мг/г відповідно для адсорбентів H-TiO₂ i Na-TiO₂. Процес адсорбції залежить від тривалості взаємодії, рівноважної концентрації йонів цирконію та кислотності розчину. Кінетика адсорбції найкраще може бути описана дифузійною кінетичною моделлю і вказує на ступінчастий характер адсорбції йонів цирконію обома адсорбентами. Рівноважну адсорбцію йонів цирконію адсорбентами H-TiO₂ i Na-TiO₂ найкраще описує теорія Ленгмюра. Із застосуванням масспектрометрії з індуктивно зв'язаною плазмою, показано, що досліджені адсорбенти селективно поглинають йони цирконію із суміші із йонами стронцію та ітрію при значенні кислотності розчину рH = 0 - 1. Відсоток вилученого цирконію із суміші складає 86,61 % для H-TiO₂ і 94,11 % для Na-TiO₂. Цей факт є дуже корисним для ядерної криміналістики а також при визначенні кількості ⁹⁰Sr у низькофонових зразках навколишнього середовища.

Ключові слова: мезопористий ТіО2, йони цирконію, адсорбція, розділення, ICP-MS.